

# NUMERICAL METHODS FOR SINGLE- AND TWO-PHASE FLOWS WITH APPLICATIONS

**UERJ** - State University of Rio de Janeiro  
**UFRJ/COPPE** - Federal University of Rio de Janeiro

**G.R. ANJOS, R. Lucena, N. Mangiavacchi, J. Pontes**

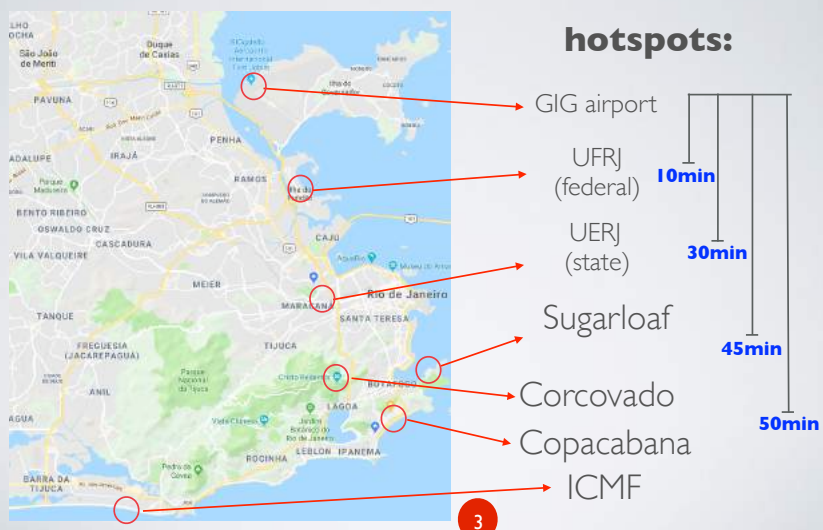
<http://www.uerj.br>      <http://2phaseflow.org>  
<http://www.gesar.uerj.br>      <http://gustavorabello.github.io>

1st ThermaSMART workshop in Tianjin - China  
 December 3rd to 5th, 2018

## OUTLINE

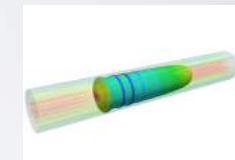
- Map of Rio de Janeiro;
- Laboratory: GESAR;
- Motivations for 1- and 2-phase flows;
- Numerical Modeling:
  - finite element method - ALE
  - interface modeling;
  - remeshing;
  - demo;
- Results and conclusions.

## RIO DE JANEIRO



## NEXT EVENTS

- International Conference on Multiphase Flows  
**19-24 May 2019, Rio de Janeiro, Brazil**  
<http://www.icmf2019.com.br>
- 4th Workshop on Advances in CFD, LB and MD Modeling of Capillary Two-Phase Flows and Experimental Validation  
**16-19 May 2019, Rio de Janeiro, Brazil**  
<http://2phaseflow.org/publicpages:events>



# GESAR LAB



<http://www.gesar.uerj.br>



Current projects sponsored by Brazilian agencies:

- Flow in Biological systems
- Cooling of electronics
- Two-phase flows
- Phase change
- Rotating disk flows

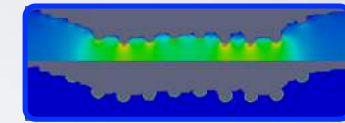
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# BACKGROUND

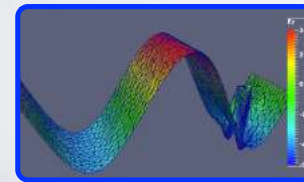


Porous Media  
**Darcy**

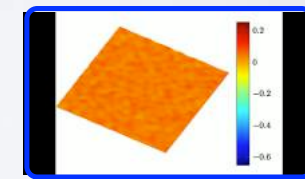
Biologic flows  
**Navier-Stokes**



Electromagnetism  
**Maxwell**



Nano-patterning  
**Kuramoto-Sivashinsky**



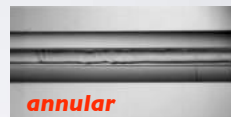
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# MOTIVATIONS



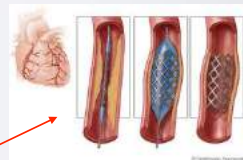
- cooling of electronics for the new generation of stack microprocessors;

microchannels with different cross-sectional geometries



- aging population and increased level of obesity ensures cardiovascular artery disease (CAD) will remain significant;

stents with different geometries



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# GOVERNING EQUATIONS



$$\frac{\partial \mathbf{v}}{\partial t} + \mathbf{c} \cdot \nabla \mathbf{v} = -\frac{1}{\rho(\phi)} \nabla p + \frac{1}{Re} \nabla \cdot [\mu(\phi)(\nabla \mathbf{v} + \nabla \mathbf{v}^T)] + \frac{1}{Fr^2} \mathbf{g} + \frac{1}{We} \mathbf{f}$$

$$\nabla \cdot \mathbf{v} = 0$$

$$\frac{\partial T}{\partial t} + \mathbf{c} \cdot \nabla T = \frac{1}{RePr} \nabla \cdot (k(\phi) \nabla T)$$

**surface tension**

ALE formulation:  $\frac{\partial \mathbf{v}}{\partial t} + (\mathbf{v} - \hat{\mathbf{v}}) \cdot \nabla \mathbf{v} \begin{cases} \hat{\mathbf{v}} = \mathbf{v} \rightarrow \text{Lagrangian} \\ \hat{\mathbf{v}} = 0 \rightarrow \text{Eulerian} \end{cases}$

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# GOV EQ - AXISYMMETRIC



$$\frac{\partial v_x}{\partial t} + \mathbf{c} \cdot \nabla v_x = -\frac{1}{\rho(\phi)} \frac{\partial p}{\partial x} + \frac{1}{Re} \mu(\phi) \nabla^2 v_x + \frac{1}{Fr^2} g_x + \frac{1}{We} f_x$$

$$\frac{\partial v_r}{\partial t} + \mathbf{c} \cdot \nabla v_x = -\frac{1}{\rho(\phi)} \frac{\partial p}{\partial x} + \frac{1}{Re} \mu(\phi) \left( \nabla^2 v_r - \frac{v_r}{r^2} \right) + \frac{1}{We} f_r$$

$$\frac{\partial v_x}{\partial x} + \frac{\partial v_r}{\partial r} + \frac{v_r}{r} = 0$$

Laplacian operator

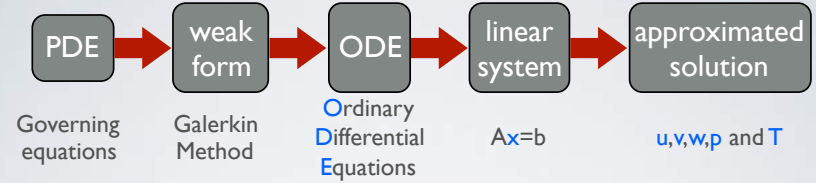
curvature

$$\nabla^2 = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r}$$

$$\kappa = \kappa_{2d} + \frac{1}{R} = \kappa_{2d} + \frac{\sin(\theta)}{r}$$

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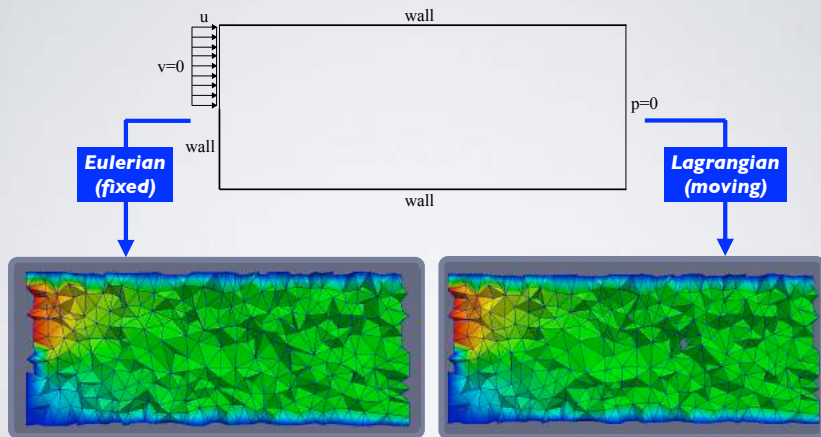
# FINITE ELEMENT METHOD



- Code's features:
- pressure, diffusive terms → Galerkin method
  - convective terms → ALE and SL methods
  - time discretization → 1st. order forward difference
  - linear systems → Projection method - LU
  - surface tension → Geometric

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# EULERIAN-LAGRANGIAN

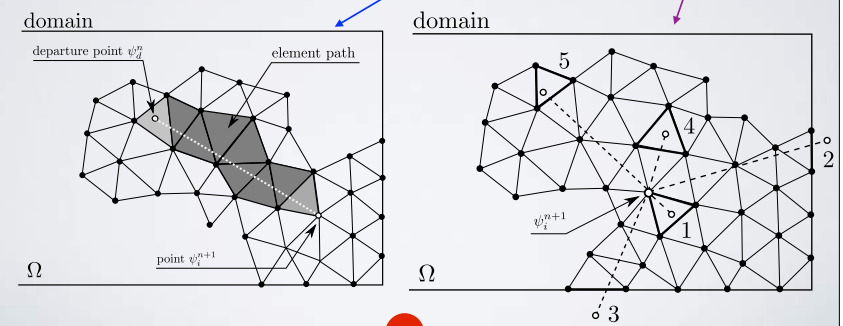


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# SEMI-LAGRANGIAN



- compute advection using fixed mesh;
- discretization of material derivative:  $\frac{D\psi}{Dt} = \frac{\psi^{n+1} - \psi^n}{\Delta t}$
- in ALE context: compute difference between flow field and node motion;
- 2-steps calculation: find departure point (trajectory) and interpolation.

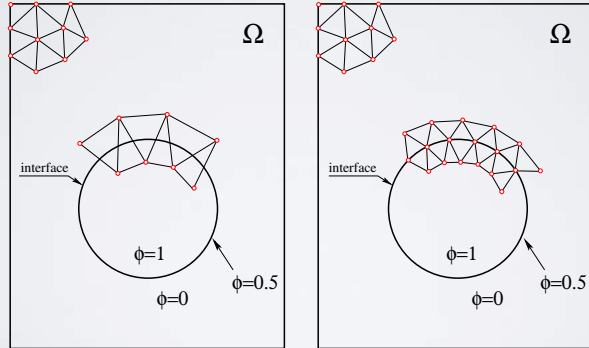


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# INTERFACE DEFINITION



- Eulerian approach: (fixed mesh)
- Lagrangian approach: (moving mesh)



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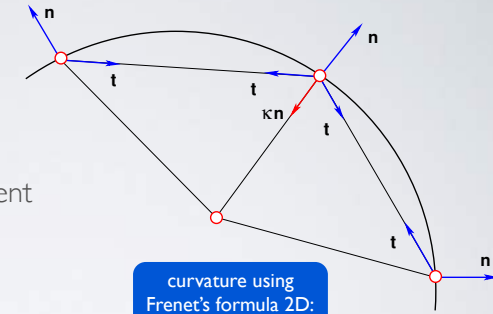
# SURFACE TENSION



$$\mathbf{f} = \sigma \kappa \mathbf{n} \delta$$

continuum surface force model  
Brackbill and Kothe (1992)

- $\sigma$  : surface tension coefficient
- $\kappa$  : curvature
- $\delta$  : Dirac delta function
- $\mathbf{n}$  : normal vector
- $\mathbf{t}$  : tangent vector
- $\phi$  : marker function (Heaviside)



curvature using Frenet's formula 2D:

$$\kappa_i = \frac{\left| \sum_{j=1}^2 \frac{t_j^2}{|t_j|} \right|}{\sum_{j=1}^2 \frac{|d_j - d_i|}{2}}$$

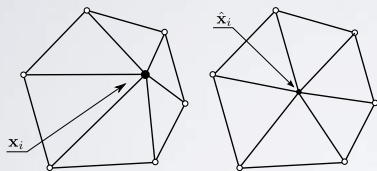
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# NODES MOTION



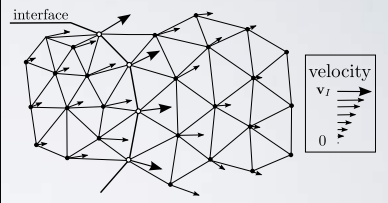
coordinates:

$$\hat{\mathbf{v}}_{e_i} = \frac{\sum_{j \in N_1(j)} e_{ij}^{-1} (\mathbf{x}_j - \mathbf{x}_i)}{dt}$$



velocities:

$$\hat{\mathbf{v}}_{v_i} = \frac{1}{n} \sum_{j \in N_1(j)} \mathbf{v}_j$$

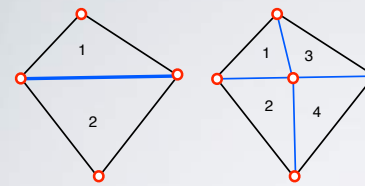


Proposed scheme:

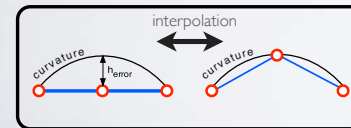
$$\hat{\mathbf{v}}(\mathbf{x}) = \begin{cases} c_1 \mathbf{v} + c_2 \mathbf{v}_v + c_3 \mathbf{v}_e & \text{if } \mathbf{x} \text{ does not belong to the interface} \\ \mathbf{v} - d_1 (\mathbf{v} \cdot \mathbf{t}) \mathbf{t} + d_2 (\mathbf{v}_e \cdot \mathbf{t}) \mathbf{t} & \text{if } \mathbf{x} \text{ belongs to the interface} \end{cases}$$

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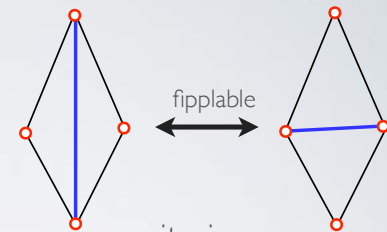
# INSERTION



2D view:



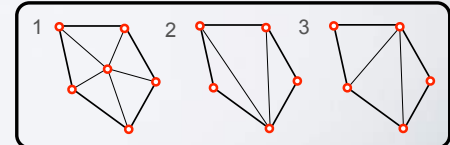
# FLIPPING



criteria:

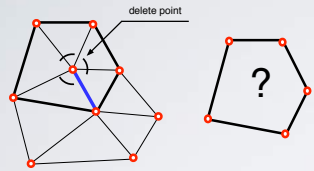
aspect ratios, curvature, area and circumcenter

example:

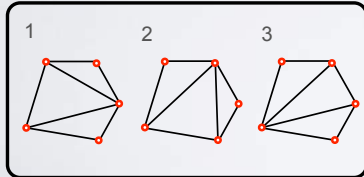


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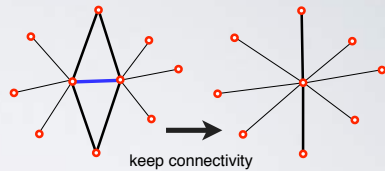
# DELETION



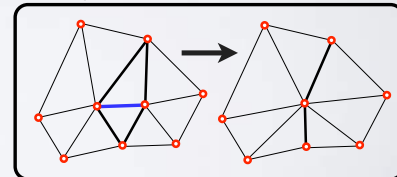
options:



# CONTRACTION



example:



# DEMO OF ALL METHODS

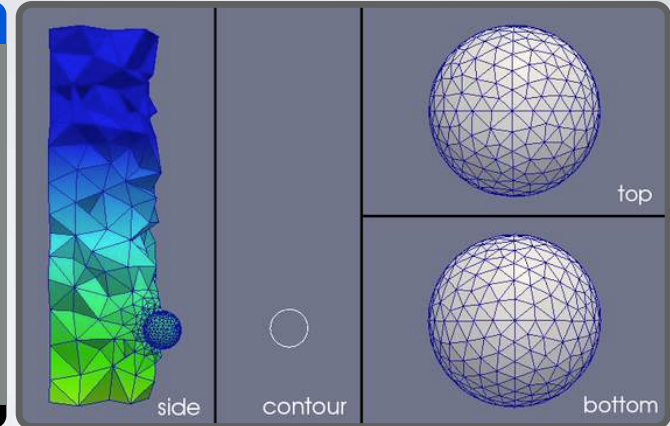
## Mesh features:

### 3d mesh

- insert/flip
- delete
- laplacian smoothing
- Helmholtz Eq.

### surface

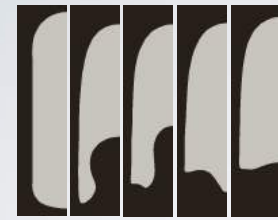
- insert/flip
- delete/contract
- smoothing
- volume conservation



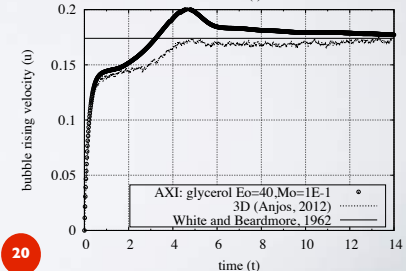
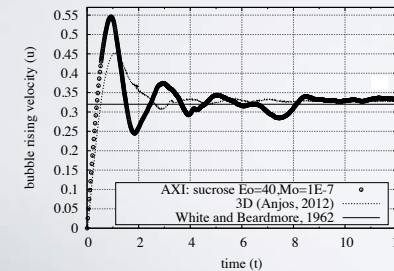
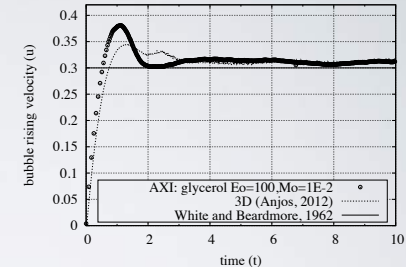
# VALIDATIONS

# AXI VALIDATIONS

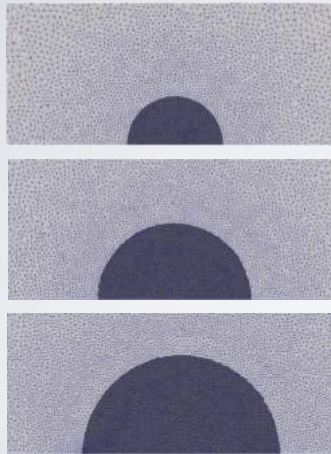
Sucrose solution:  
 $Mo = 1e-7$   
 $Eo = 40$



time

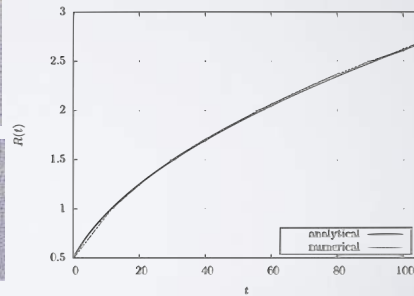


# AXI PHASE CHANGE



Evaporating drop  
in superheated liquid

Moving mesh method for direct numerical simulation of two-phase flow with phase change (E. Gros, G. Anjos, J. Thome, 2018)



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# AXI VALIDATIONS



Rising bubbles: **interface tracking, surface tension, gravity**

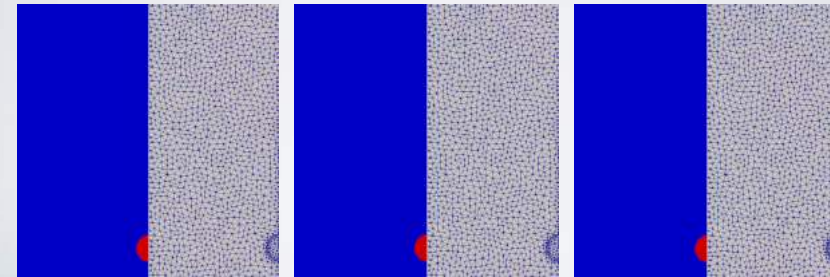
$$\rho_{in} = 1.225 \text{ kg/m}^3 \quad \mu_{in} = 1.78 \cdot 10^{-5} \text{ Pa}\cdot\text{s}$$

$$\rho_{out} = 1350 \text{ kg/m}^3 \quad We = 115.662$$

case 1  
 $\mu_{out} = 2.73 \text{ Pa}\cdot\text{s}$   
 $N = 42.895$

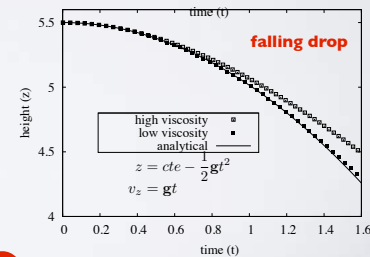
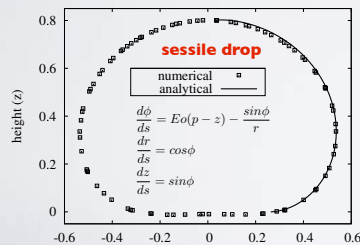
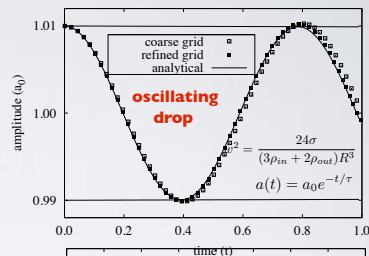
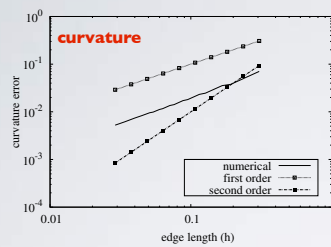
case 2  
 $\mu_{out} = 1.28 \text{ Pa}\cdot\text{s}$   
 $N = 194.88$

case 3  
 $\mu_{out} = 0.539 \text{ Pa}\cdot\text{s}$   
 $N = 1091.57$



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# 3D VALIDATIONS



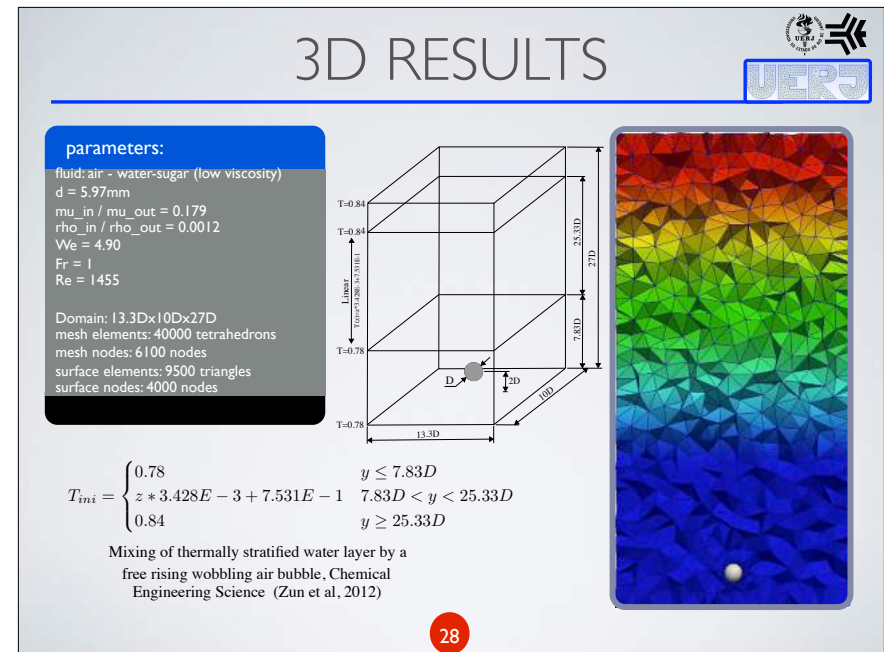
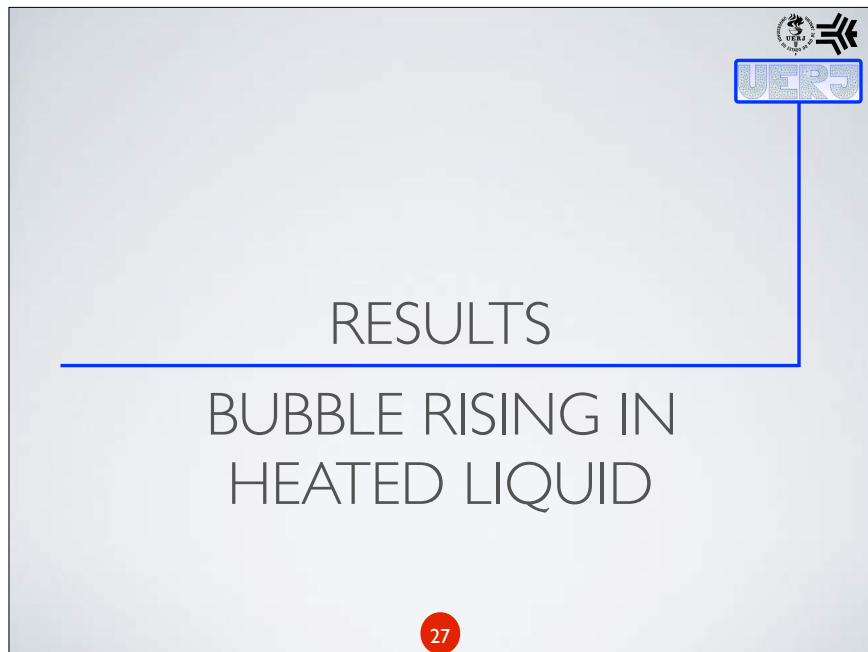
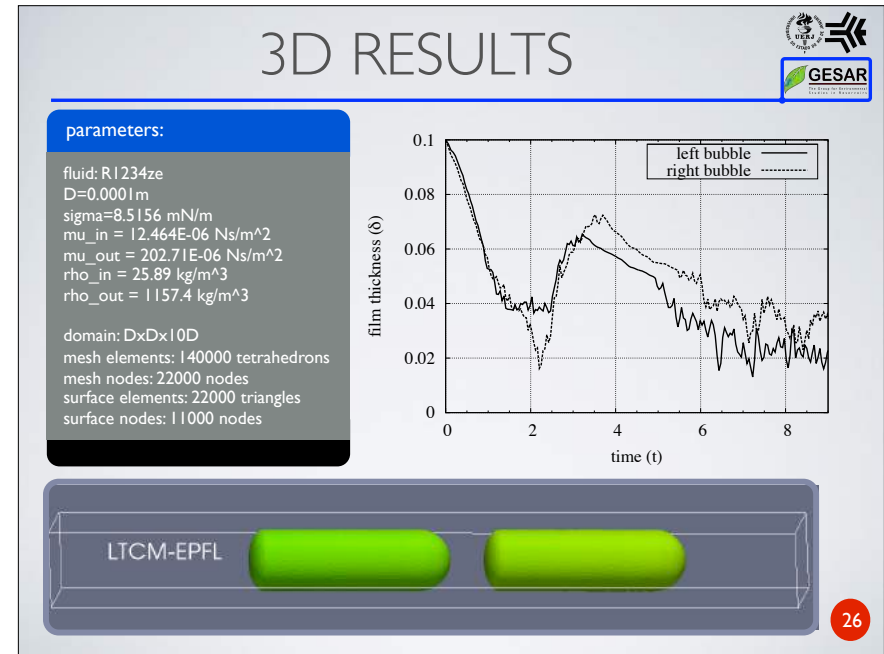
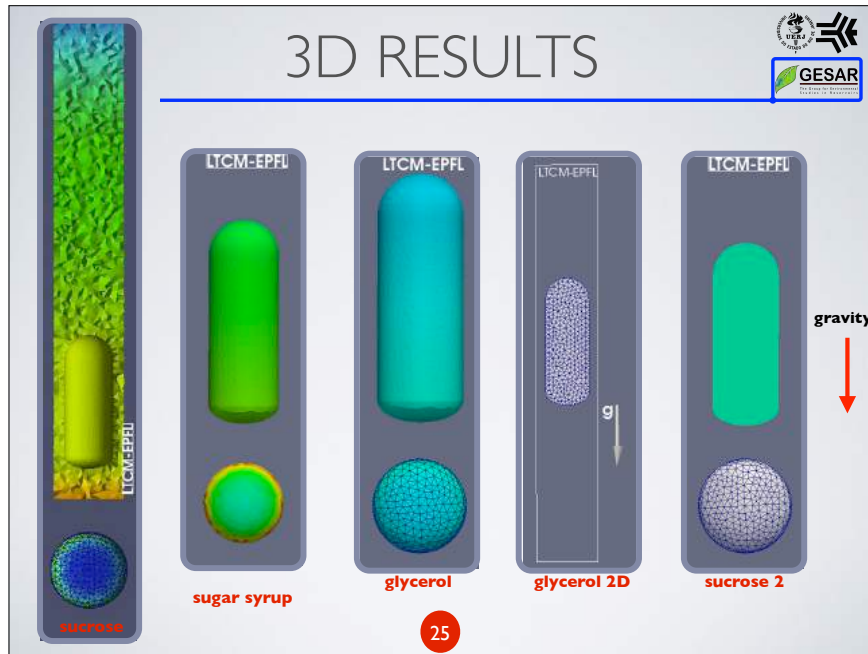
Anjos et al., JCP, 2014 - published

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# RESULTS

3D CASES FOR TAYLOR  
BUBBLES AND SLUG  
FLOWS

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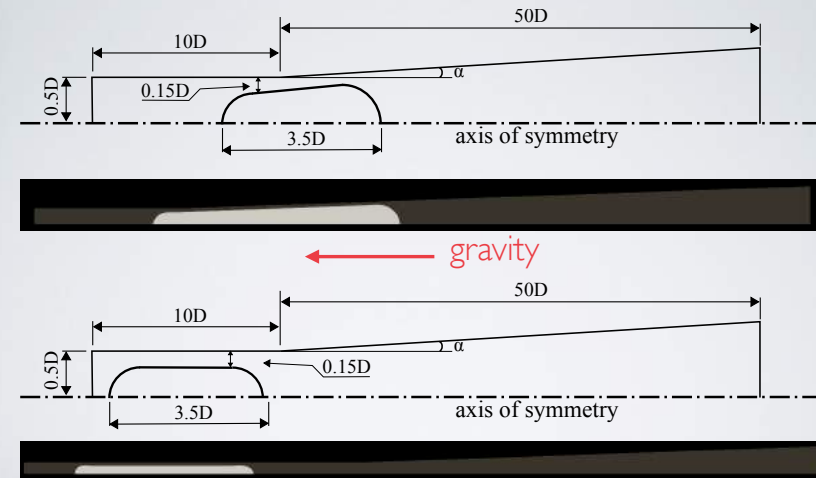


## RESULTS

TAYLOR TO SPHERICAL  
CAP TRANSITION IN  
DIVERGENT CHANNEL

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## AXI RESULTS: DW+G



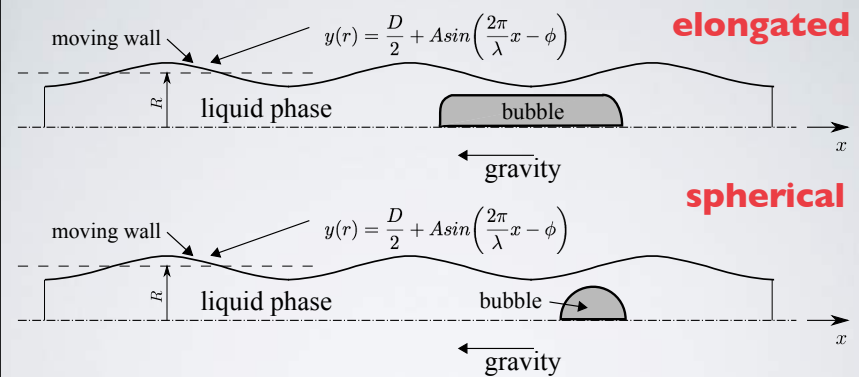
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## RESULTS

SINUSOIDAL CHANNEL

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## GEOMETRIES



$$\text{wall moves as: } y(r) = \frac{D}{2} + A \sin \left\{ \frac{2\pi}{\lambda} (x - x_c) - \phi \right\}$$

where  $x_c$  is bubble's centroid position

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# RESULTS: BUBBLE SHAPE



DEGG3 - Diethylene-glycol, higher inner viscosity



DEGG11 - Diethylene-glycol



DEGG3 - Diethylene-glycol, higher inner viscosity



# PROJECT OUTPUT

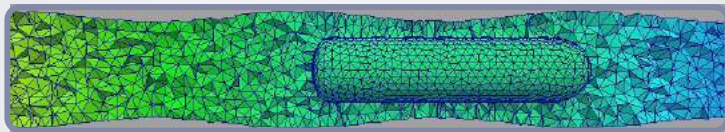
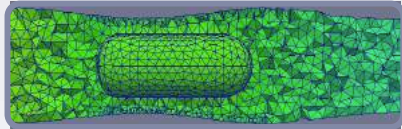


- Strong numerical background for several applications, including cooling of electronics, rotating disk, pattern formation, corrosion, electromagnetism etc.
- Development of analytical mathematical models and inverse problems to provide reliable estimates of physical parameters in single- and two-phase flow systems;
- Establish a sustainable cooperation between researchers from PPG-EM/UERJ, COPPE/UFRJ (Brazil) and ThermaSMART partners for single- and two-phase flows problems, including porous media.



# THANK YOU!

<http://gustavorabello.github.io>



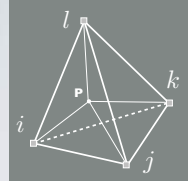
THANKS TO:



# FINITE ELEMENT METHOD



volume coordinates:



$$L_i = \frac{V_i}{V} \quad L_j = \frac{V_j}{V}$$

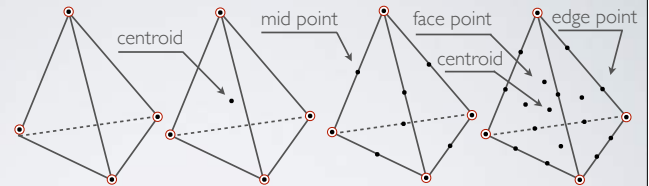
$$L_k = \frac{V_k}{V} \quad L_l = \frac{V_l}{V}$$

$$x = L_i x_i + L_j x_j + L_k x_k + L_l x_l$$

$$y = L_i y_i + L_j y_j + L_k y_k + L_l y_l$$

$$z = L_i z_i + L_j z_j + L_k z_k + L_l z_l$$

linear element    mini element    quad element    cubic element



○ pressure, temperature    • velocity

finite elements:

element:	nodes:	LBB:	lin sys:
linear	4	unstable	small
mini	5	stable	moderate
quad	10	stable	large
quad+bubble	11	stable	large
cubic	20	stable	very large